Study of Plate Cheravon Heat Exchangers by CFD Analysis

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Abstract - Plate heat exchangers phes are used in a variety of chemical, process, and power industries over a broad range of temperatures due to their compactness, ease of maintenance, flexibility, and favorable thermal-hydraulic characteristics. We designed the PHE's by elivating the angle of grooves to 30 degrees and 60 degrees. The grooves will make on the heat exchangers by changing the L-angle. The analysis done by using the catiaand ANSYS(FLUENT module) softwares. To analyze the velocity counters and path lines and the pressure variations and the temperature variation all along the plate to achieve the required temperature difference.

keywords: cfd anlysis , plate heat exchangers, h-plate.

I. INTRODUCTION

Heat exchangers are mainly used in refrigerators, turbines, boilers. These are of many types. Among them plate heat exchanger is mainly used.Plate heat exchanger is used for reduce the temperature of hot fluid in system. By passing the cold fluid around the tubes the temperature will be reduced. The efficiency will be based on heat transfer rate, temperatures of fluids. CFD (Conjugated Fluid Dynamics) analysis on plate heat exchanger is done by making the "grooves" on the plate. The analysis of heat exchangers is done for decreasing the velocity of fluid flow in the exchanger. The plate heat exchangers are prepared by using aluminum and steel.

II. METHODOLOGY

ANALYSIS

There are 2 types of analysis mainly, --Real type analysis Software analysis

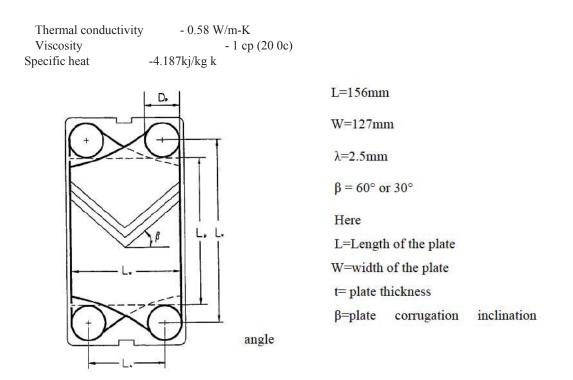
3D modeling, constraints, meshing, parameters, result.

PARAMETERS

Flow rate of fluid, temperature, diameter of tube, density of fluid, length, specific heat of fluid, mass flow rate, pressure, velocity.

PROPERTIES OF FLUID

Mostly in heat exchangers water is used as a fluid. Density of fluid (water) -1000kg/cu.m Room temperature - 27 0c Boiling point - 100 0c Freezing point - 0 0c



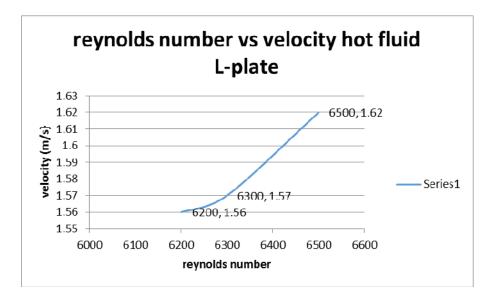
III. CALCULATIONS

$$\operatorname{Re} = \frac{\text{inertial forces}}{\text{viscous forces}} = \frac{\rho \mathbf{v}L}{\mu} = \frac{\mathbf{v}L}{\nu}$$

Reynolds number, Diameter of tube = 4mm Dynamic Viscosity (water) = 1.002×10^{-3} Kg/M-sec

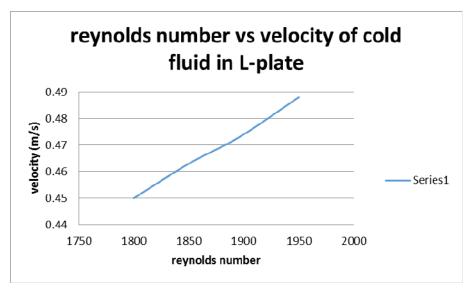
FOR HOT WATER

For Re= 6100 Velocity V= $(1.002 \times 10^{-3} \times 6100)/4$ V= 1.528 M/s Similarly Re= 6200 , then V= 1.56 Re= 6300 , then V= 1.578 Re= 6500 , then V= 1.628



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FOR COLD WATER
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For Re= 1800	
$V = (1.002 \times 10^{-3} \times 1800)/4$	
Velocity V= 0.45	
Similarly Re= 1850	,then V= 0.463
Re= 1896	,then V= 0.474
Re= 1950	,then V= 0.488



PECLET NUMBER (Pe)

Pe= convective flux/ conductive flux

$$P_e = \frac{uD_h}{\alpha}$$
, $\alpha = \frac{k}{\rho c_p}$

For water $\mu = 1.002 \times 10^{-3}$

K = 0.58 W/M-K Sp Heat= 4.187 Kj/Kg-K Density (water)= 1000Kg/cu.m

Now,
$$\alpha = 0.58/(1000x4.187x1000)$$

= $1.385x10^{-7}$
Pe = $(1.002x10^{-3}x4x10^{-3})/1.385x10^{-7}$
Pe = 0.0289

NUSSELT NUMBER

Nu= 0.26x Pe^{0.27} Nu= 0.26x 0.0289^{0.27} Nu= 0.099

HEAT TRANSFER CO-EFFICIENT

 $h = \frac{Nu k}{D_h}$ = (0.099x0.58)/ 4x10⁻³ h = 14.35 W/sq.m-K

TURBULENT FRICTION FACTOR

 $f = 2.9 x P e^{-0.13}$ = 2.9x0.0289^{-0.13} f= 4.597

PRESSURE DROP

$$\Delta P = f\left[\frac{LG^2}{2D_h \rho g_c}\right]$$

 $\begin{array}{l} g=9.81 \ \text{Kg/cu.m} \\ G= (\text{density x volume})/ \ \text{area} \\ = (1000 \ \text{x} \ 156 \text{x} \ 127 \text{x} 2 \text{x} \ 10^{-6}) \\ = 156 \\ \end{array}$ Specific mass flow rate (G) = 156 \ \text{Kg/Sq.m-sec} \end{array}

$$P = 4.597*[(156*10^{-3}*156^{2})/(2*4*10^{-3}*1000*9.81]$$

Therefore pressure drop = 222.376

IV. CFD ANALYSIS ON PLATE HEAT EXCHANGER

plate heat exchangers on l-plate (30 degrees) velocity path lines

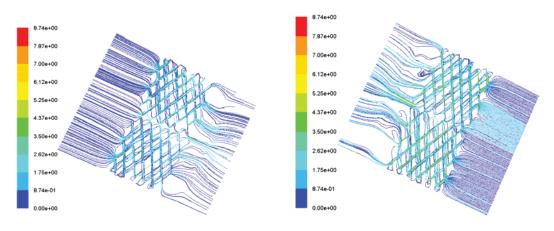


fig a : velocity pathlines of cold and hot side

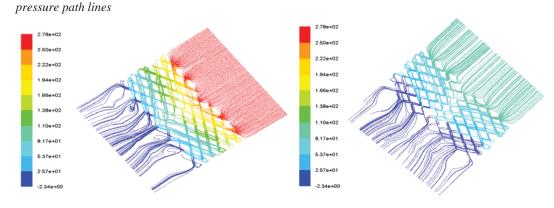
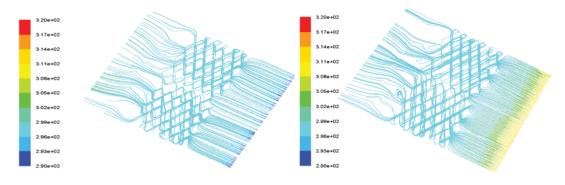


fig ${\sf b}$: pressure pathlines on hot and cold water



$temperature \ pathlines$

fig c temperature path- lines on hot and cold side

Cfd Analysis On Plate Heat Exchangers Of 60 Degree Plate (H-Plate)

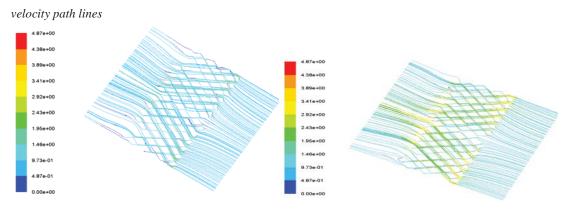
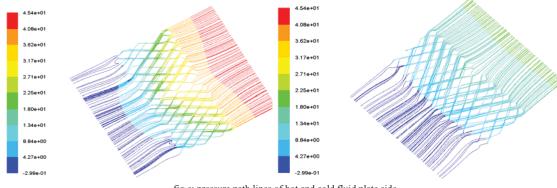
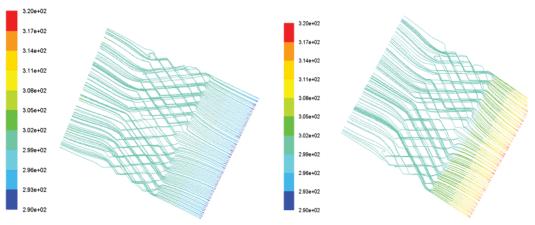


fig d : velocity path lines of cold and hot plate side



pressure path lines

fig e: pressure path lines of hot and cold fluid plate side



temperature pathlines

fig f : temperature path lines of cold and hot fluid plate side

V. CONCLUSION

The two plate heat exchangers are considered and the cfd analysis has been done and obtained the velocity pressure and temperature distribution on overall plates are determined and the calculation has done on the l-plate and the h-plate and the variation of the velocity and the pressure results the friction factor high in the l-

plate but the heat transfer rate is more occupied and the distributed all along the h- plate which having higher efficiency.

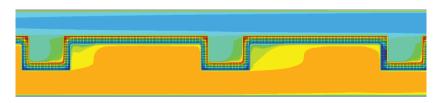


fig : temperature distribution on plate heat exchanger on L-plate

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